
MANAGING LIQUOR CHEMISTRY TO OPTIMIZE PRODUCTION, QUALITY AND EFFICIENCY

MICHAEL KJERULF

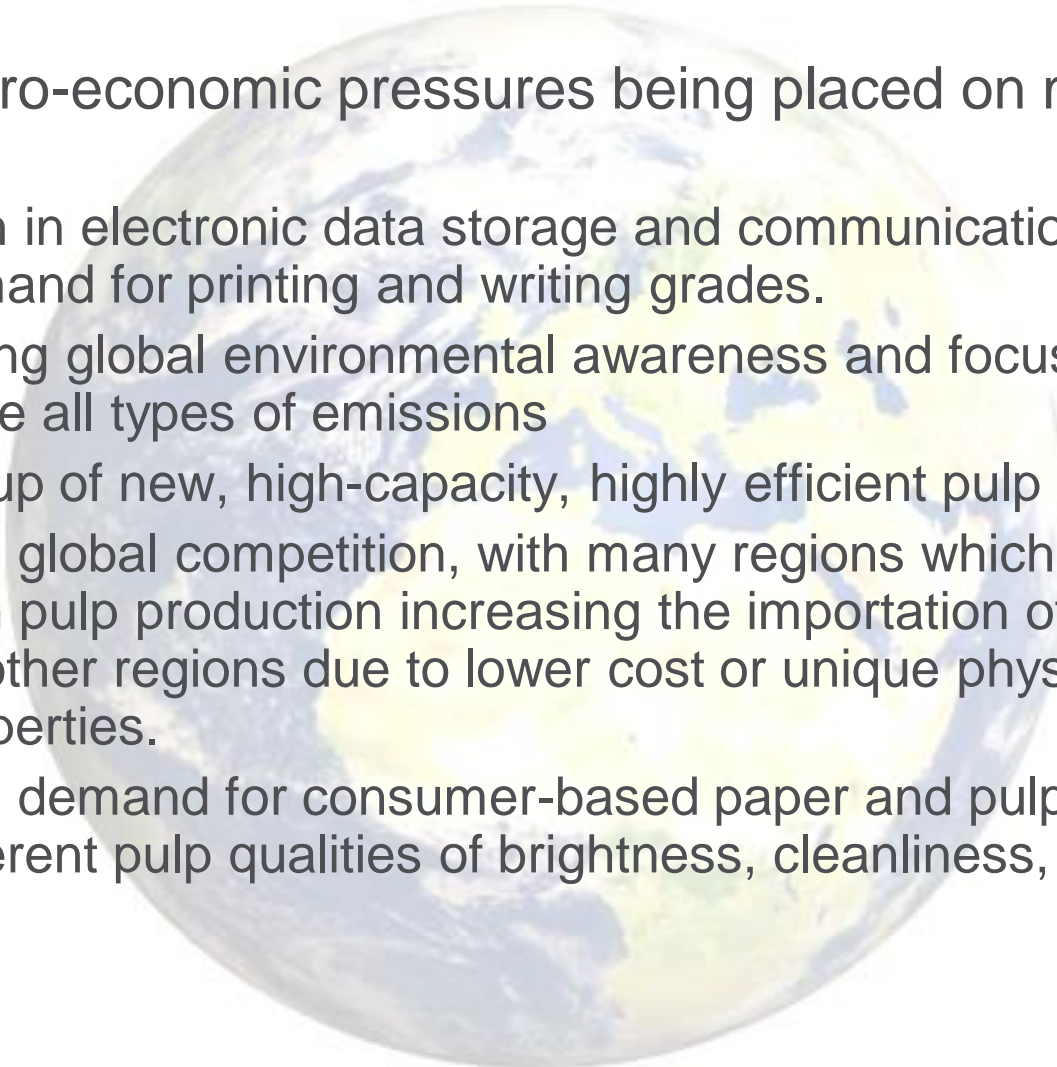
INDUSTRY TECHNICAL CONSULTANT, PULP AND RECOVERY,

March 2020

Topics

- 1) The Need for Liquor Chemistry Management
- 2) Carbonate Loading in the Liquor Process
- 3) Sulfate Loading in the Liquor Process
- 4) Organic Carryover and Deposition
- 5) Concentration of Non-Process Elements
- 6) Case Study
- 7) Summary

The Need for Liquor Chemistry Management

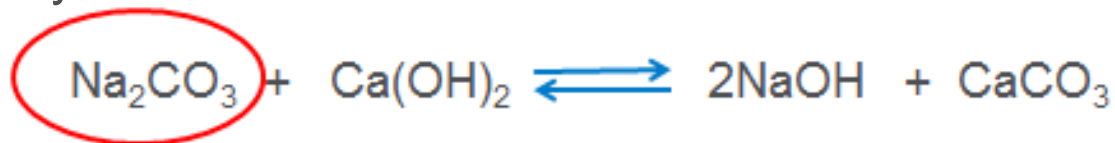
- 
- ▲ Changing macro-economic pressures being placed on mills in all regions:
 - 1. The growth in electronic data storage and communication, reducing demand for printing and writing grades.
 - 2. The growing global environmental awareness and focus, forcing mills to reduce all types of emissions
 - 3. The start-up of new, high-capacity, highly efficient pulp mills
 - 4. Increasing global competition, with many regions which had been self-reliant on pulp production increasing the importation of pulp produced in other regions due to lower cost or unique physical and chemical properties.
 - 5. Increasing demand for consumer-based paper and pulp products, requiring different pulp qualities of brightness, cleanliness, etc.

The Need for Liquor Chemistry Management

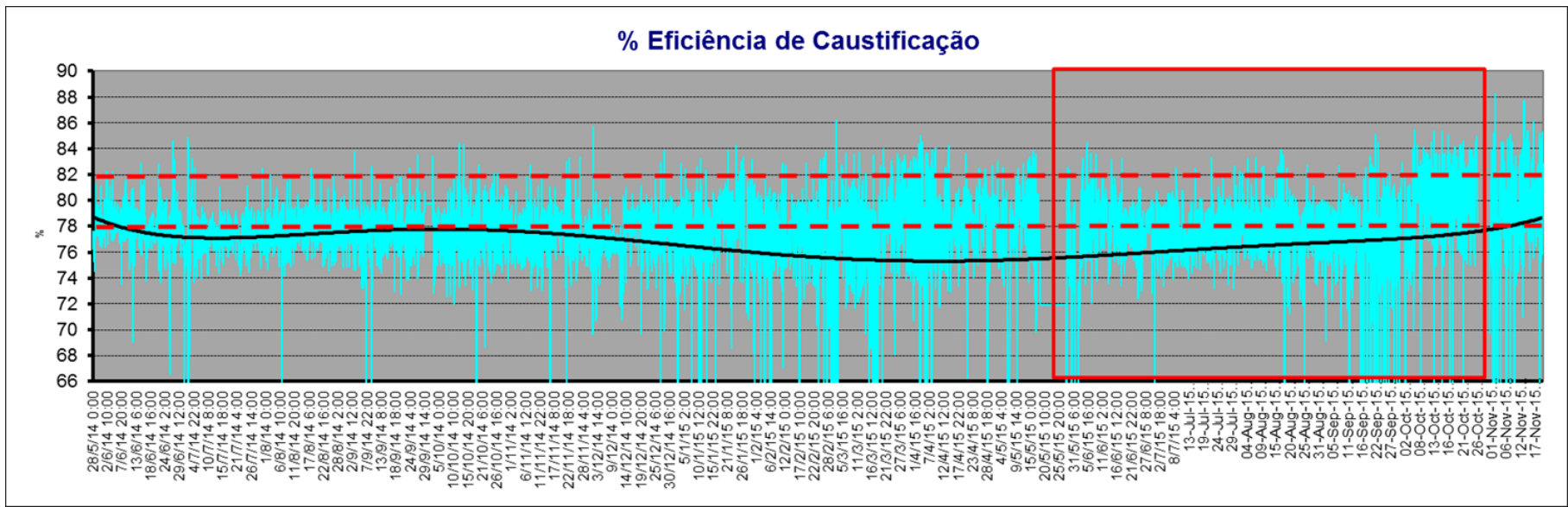
- ▲ These macro-economic demands put competing pressures on mills:
 - 1. Reduce operating costs – use of lower quality or more juvenile wood, less operators/managers/lab personnel, extended operating campaigns
 - 2. Increase production – operating beyond design capacities, particularly in liquor processing areas, higher strain on effluent and influent treatment areas. All done without capital investment
 - 3. Reduce emissions – additional water re-use to reduce the amount of water discharged, tighter operating controls on air emissions.
- ▲ All of these changes are causing significant chemistry changes to the entire liquor process, increasing deposition, reducing operating efficiency, and increasing costs!!

Carbonate Loading in the Liquor Process

- ▲ Primary ion which builds up in process, can cause scaling/deposition and lost efficiency!
- ▲ Increases due to failure to optimize and maintain % Causticizing Efficiency.



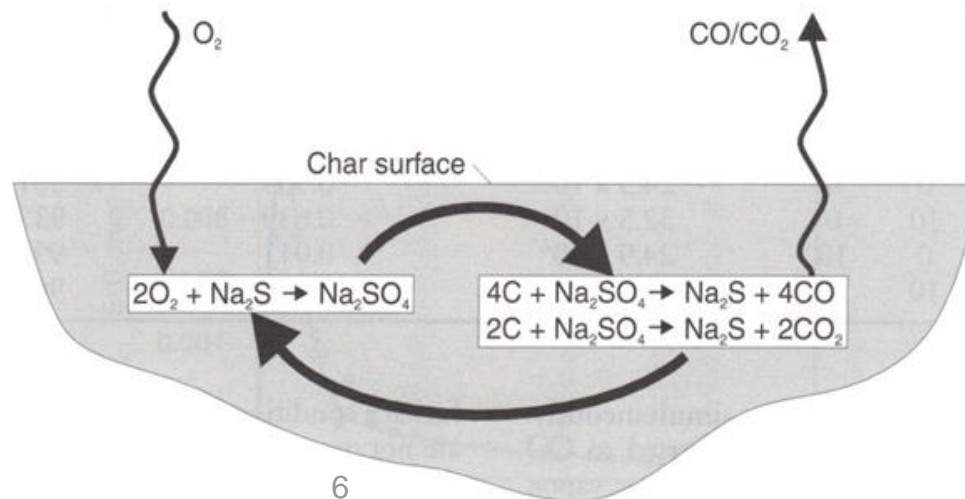
- ▲ Variation and low %CE results increase carbonate throughout entire liquor process due to disassociation of sodium carbonate!



Sulfate Loading in the Liquor Process

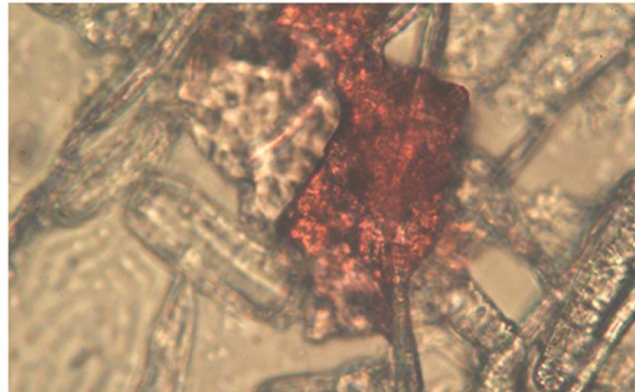
- ▲ Failure to control sulfate levels in the liquor can result in scale formation (calcium sulfate, barium sulfate, burkeite/dicarbonate, etc.) and increase operating costs due to high non-process element loading.
- ▲ Sulfate level is controlled almost completely by Reduction Efficiency of the Recovery boiler.
- ▲ Changing environmental restrictions, loading increases on boilers, etc. all can reduce % Reduction Efficiency.

Figure 6-4. The sulfate-sulfide cycle.



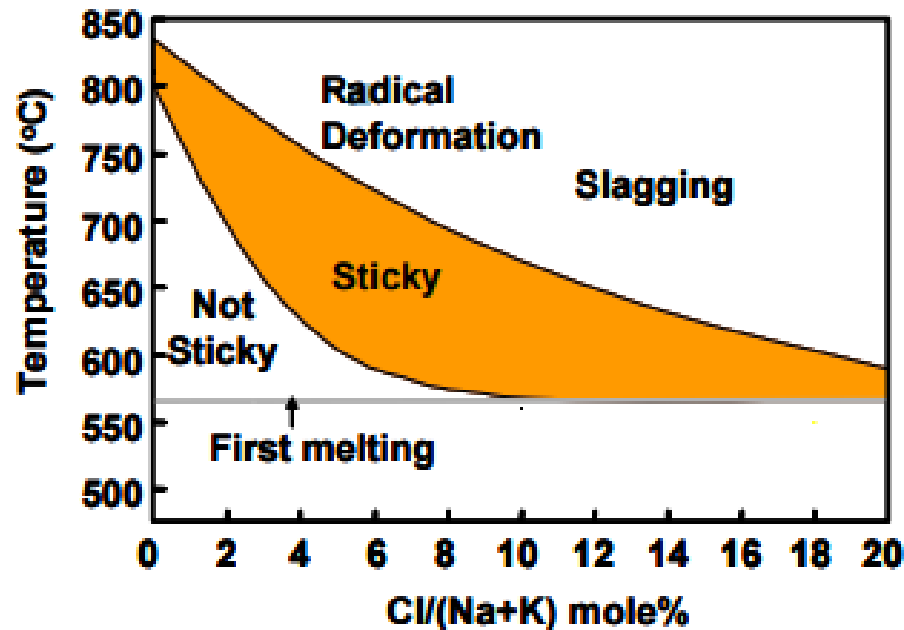
Organic Carryover and Deposition

- ▲ There are a number of items which impact organic deposition or high COD to effluent:
 - 1. Cooking uniformity – Reduces uncooked wood shives, liberates encapsulated pitch from the fiber and into the liquor to be washed.
 - 2. Residual alkalinity control – since most organics are soluble under alkaline conditions, maintaining alkaline levels throughout the washing process is critical to take advantage of natural removal!
 - 3. Brown Stock Washing Efficiency – maximum washing efficiency, combined with proper residual alkalinity control, will remove most of the organic materials present.
 - 4. Stabilizing ions – minimizing calcium and silica in particular is critical – bark removal and % Causticizing Efficiency!



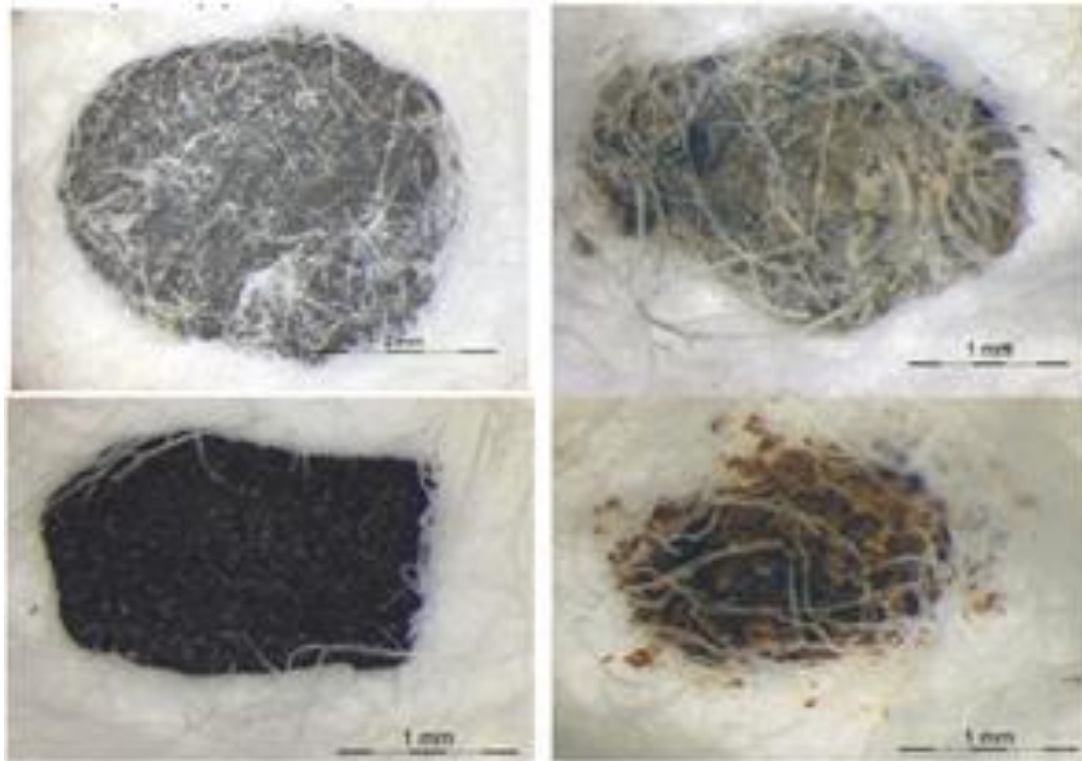
Concentration of Non-Process Elements

- ▲ Over time, if sulfate, carbonate, and other non-process elements (chlorides, potassium, silica, etc.) are not controlled, they will concentrate due to reduced discharge or “cycling up”.
 - Normally results in formation of deposits (burkeite, calcium carbonate, calcium silicate, etc.), plugging in the Recovery Boiler draft (due to reduced “sticky temperature” from chlorides/potassium), etc.



Case Study

- ▲ **Background:** European mill struggled with high “dirt” count in sheet forcing downgrade of 5-8% of all pulp produced each month. Multiple project teams, focus groups, etc. but could not resolve despite process changes to washing and bleaching.



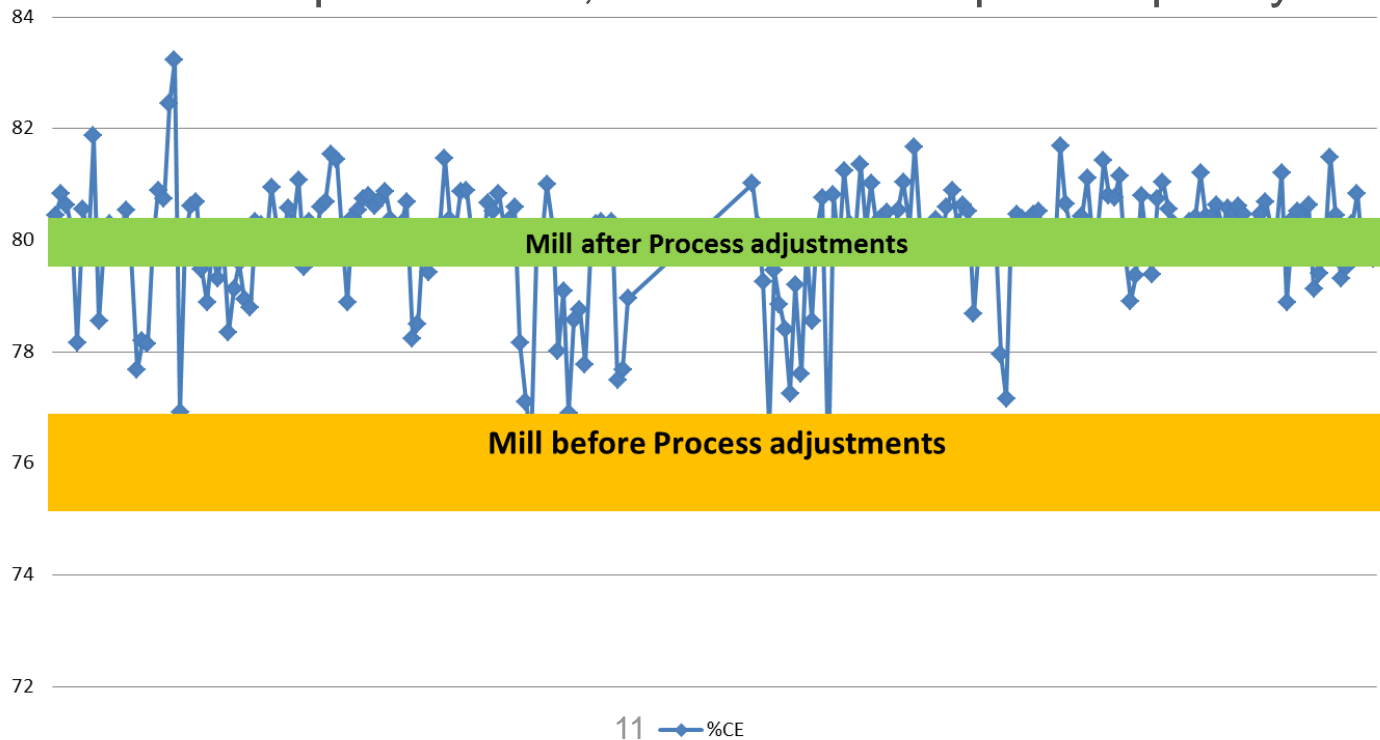
Case Study

- ▲ Completed liquor process analysis and review. Samples taken:
 - Wood chips being fed to the digester
 - Black Liquor – Weak, Intermediate, and Burning Liquors
 - Green Liquor – Clarified, Unclarified, GL Dregs
 - White Liquor – Clarified, Unclarified
 - Lime/Lime Mud – Reburned Lime, Purchased Lime, Mud to Lime Kiln
- ▲ Also inspected system during annual outage.



Case Study

- ▲ Identified three areas of correction based on information:
 - Improve % Causticizing Efficiency to reduce carbonate-based scale
 - Change wash aid to reduce polydimethyl siloxane (PDMS) carryover
 - Improve alkalinity control to improve organic washing.
- ▲ Initial focus was to improve %CE, which was completed quickly



Case Study

- ▲ Next, made slight adjustments to continuous digester alkalinity profile to increase alkalinity of blown pulp.
- ▲ Finally replaced wash aid with highly dispersible, lower-molecular weight silicone formulation.
- ▲ **FINAL RESULTS: *Increased average First Quality pulp to in excess of 99%.***

Summary

- ▲ With mills facing additional pressures to reduce costs and meet ever-tightening environmental restrictions, it is critical that the chemistry of the entire liquor cycle be closely monitored and controlled.
- ▲ Failure to control the liquor chemistry will result in:
 - Decreased operating efficiency
 - Increased product quality issues
 - Reduced production
 - Increased costs of operation.
- ▲ Chemistry issues often are not found in the area where the issue is first noted, so evaluation of the entire process is mandatory to solve issues that arise.

Questions???

