

# **E<sub>OP</sub> Stage control**

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# $E_{OP}$ stage pH control: why do it?

- Significant savings in NaOH if end pH can be lowered without affecting brightness
  - Target reduction from 10.8 to 10.3 results in ~2.0-2.5kg/ton NaOH saving
  - At ~0.50\$/kg NaOH, this represents ~330,000-410,000\$/yr for a 1000 bdmt/d.

# $E_{OP}$ stage pH control: other incentives?

- Temperature affects how pH of  $E_{OP}$  filtrate behave
  - This is not temperature correction for the pH probe electronics
  - This is temperature compensation of solution
- Safety issue
  - Insertion/retraction of pH probe
  - Hot process media
  - High pH

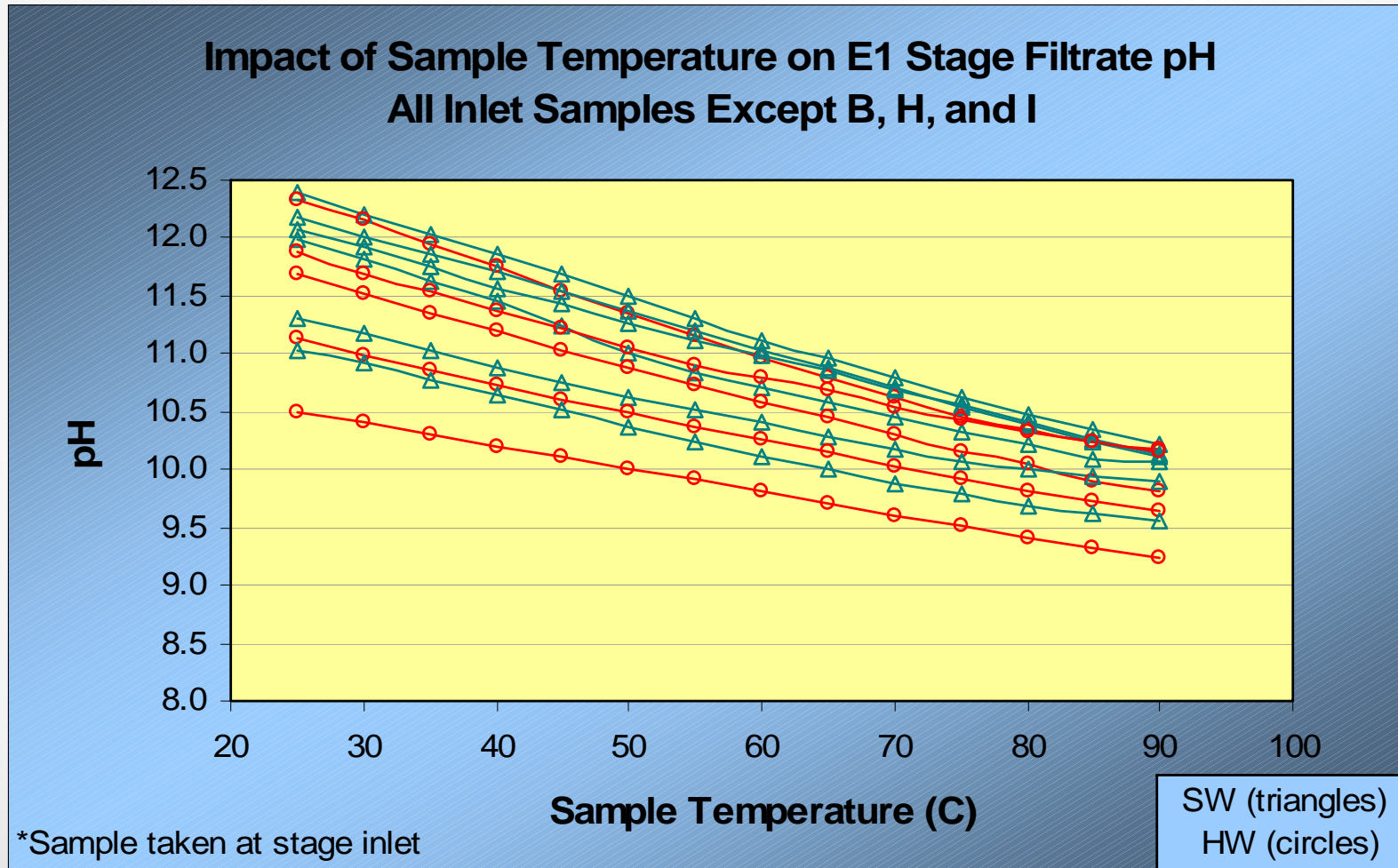
# $E_{OP}$ stage pH control: other incentives?

- Simplify and speed up preventive maintenance
  - Typically a long process for calibration
  - Insertion pH probe tends to have short life span (due to high temp, high pH, scaling)
  - Become insensitive with time (due to high temp, high pH, scaling)
  - Calibration accuracy
    - Measure in medium consistency pulp, calibrate in liquid

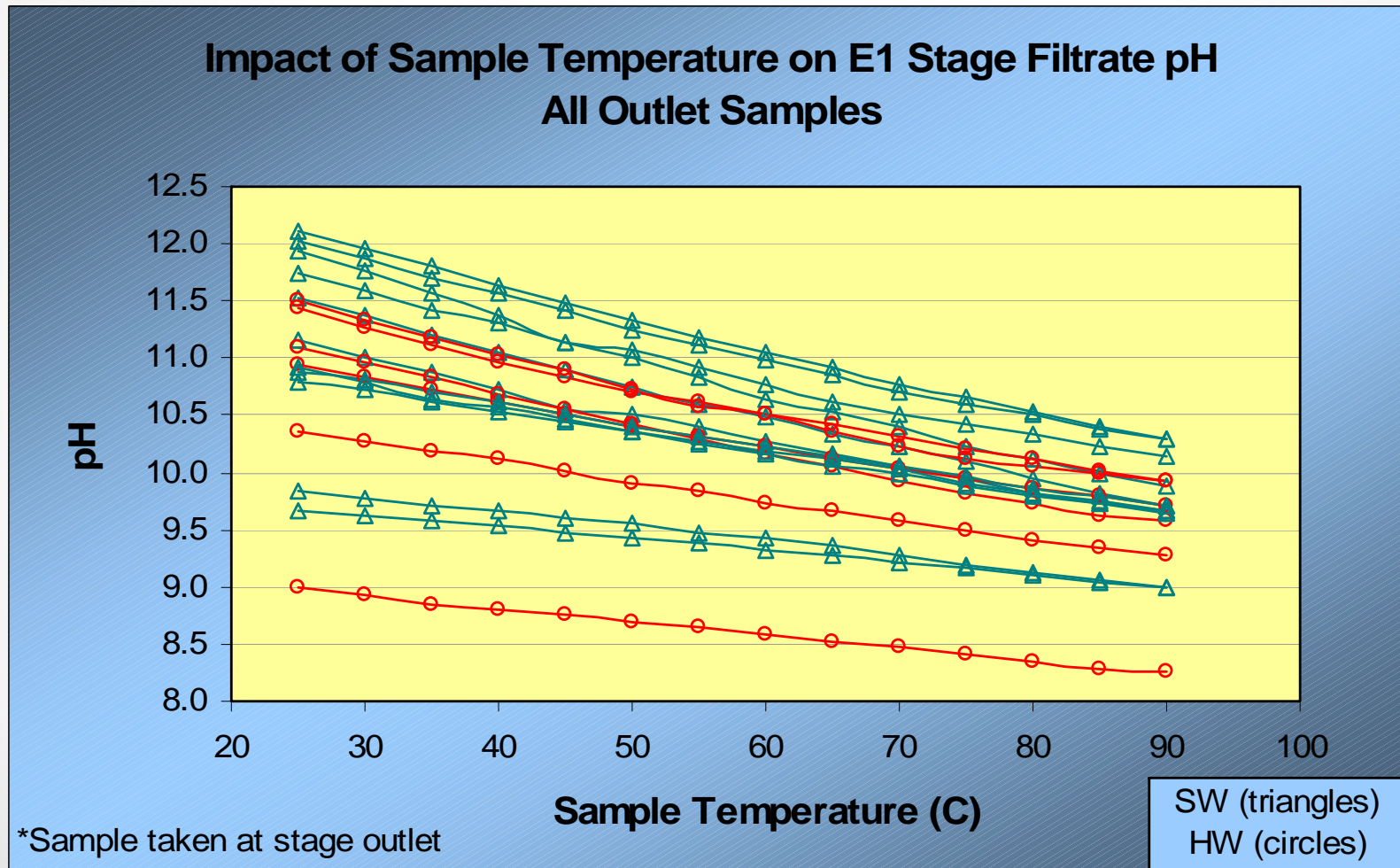
# $E_{OP}$ stage pH control: correction at 25°C

- Standardization at 25°C:
  - Report pH meter at 25°C at operator level
  - Report lab test at 25°C to the operator
    - Recommended to enter test results for pH & temperature in DCS for computation using same DCS compensation
  - Recommended 25°C because this is how pH are reported in technical papers by research facilities such as FPIinnovations
  - Allow comparisons from mill to mill
    - *However, any fixed temperature standardization would work...*
- Works for  $O_2$  stages &  $E_{OP}$  stages of hardwood and softwood

# $E_{OP}$ stage pH control: correction at 25°C



# $E_{OP}$ stage pH control: correction at 25°C



# E<sub>OP</sub> stage pH control:

Correction Table for E1 Stage Inlet pH

correction at 25°C

Sample Temperature (C)										pH Corrected to 25 C	
90	80	70	60	55	50	45	40	35	30		
6.00	6.00	6.00	6.00	6.00	6.00	6.00	6.00	6.00	6.00	6.00	
7.00	7.00	7.00	7.00	7.00	7.00	7.00	7.00	7.00	7.00	7.00	
1. Temperature of Sample					8.00	8.00	8.00	8.00	8.00	8.00	
					9.00	9.00	9.00	9.00	9.00	9.00	
9.02	9.05	9.07	9.09	9.09	9.09	9.10	9.10	9.10	9.10	9.10	
9.09	9.13	9.16	9.18	9.19	9.19	9.19	9.20	9.20	9.20	9.20	
9.15	9.20	9.24	9.27	9.28	9.29	9.29	9.30	9.30	9.30	9.30	
9.20	9.26	9.32	9.36	9.37	9.38	9.39	9.39	9.40	9.40	9.40	
9.25	9.32	9.38	9.44	9.45	9.47	9.48	9.49	9.49	9.50	9.50	
9.28	9.36	9.44	9.51	9.53	9.55	9.57	9.58	9.59	9.60	9.60	
9.31	9.40	9.49	9.57	9.61	9.63	9.66	9.67	9.69	9.69	9.70	
9.33	9.43	9.54	9.63	9.67	9.70	9.74	9.76	9.78	9.79	9.80	
9.35	9.45	9.57	9.68	9.73	9.77	9.81	9.84	9.87	9.89	9.90	
9.37	9.48	9.60	9.72	9.77	9.83	9.88	9.92	9.95	9.98	10.00	
9.38	9.49	9.63	9.76	9.82	9.88	9.94	9.99	10.03	10.07	10.10	
9.39	9.51	9.65	9.79	9.85	9.92	9.99	10.05	10.11	10.16	10.20	
9.40	9.52	9.67	9.82	9.89	9.96	10.04	10.11	10.18	10.24	10.30	
9.41	9.54	9.68	9.84	9.91	10.00	10.09	10.17	10.25	10.33	10.40	
9.42	9.55	9.70	9.87	9.95	10.04	10.13	10.22	10.32	10.41	10.50	
9.43	9.56	9.72	9.89	9.98	10.08	10.18	10.28	10.39	10.49	10.60	
9.44	9.57	9.74	9.92	10.01	10.12	10.23	10.34	10.46	10.58	10.70	
9.46	9.59	9.76	9.95	10.05	10.16	10.28	10.41	10.54	10.67	10.80	
				2. pH of Sample		10.09	10.21	10.34	10.48	10.62	10.76
						10.14	10.27	10.41	10.56	10.71	10.86
						3. pH corrected to 25 C				11.00	
9.51	9.66	9.85	10.08	10.20	10.33	10.47	10.62	10.77	10.92	11.10	
9.53	9.69	9.90	10.14	10.26	10.41	10.57	10.72	10.88	11.04	11.20	
9.56	9.73	9.95	10.20	10.34	10.49	10.65	10.81	10.98	11.14	11.30	
9.60	9.77	10.01	10.28	10.42	10.57	10.74	10.91	11.08	11.24	11.40	
9.64	9.83	10.07	10.36	10.50	10.66	10.84	11.00	11.17	11.34	11.50	
9.69	9.89	10.15	10.44	10.59	10.76	10.93	11.10	11.27	11.44	11.60	
9.75	9.96	10.23	10.53	10.69	10.85	11.03	11.20	11.37	11.54	11.70	
9.82	10.04	10.32	10.63	10.78	10.95	11.13	11.30	11.47	11.64	11.80	
9.90	10.12	10.41	10.72	10.88	11.05	11.23	11.40	11.57	11.74	11.90	
9.98	10.21	10.50	10.82	10.98	11.14	11.33	11.50	11.67	11.84	12.00	
10.07	10.30	10.60	10.92	11.08	11.24	11.43	11.60	11.77	11.94	12.10	
10.16	10.40	10.70	11.02	11.17	11.34	11.52	11.70	11.87	12.04	12.20	
10.26	10.50	10.80	11.12	11.27	11.44	11.62	11.80	11.97	12.14	12.30	
10.35	10.59	10.90	11.22	11.37	11.54	11.72	11.90	12.07	12.24	12.40	
10.45	10.69	11.00	11.32	11.47	11.64	11.82	12.00	12.17	12.34	12.50	
10.55	10.79	11.09	11.42	11.57	11.74	11.92	12.10	12.27	12.44	12.60	
10.65	10.89	11.19	11.52	11.67	11.84	12.02	12.20	12.37	12.54	12.70	
10.75	10.99	11.29	11.62	11.77	11.94	12.12	12.30	12.47	12.64	12.80	
10.85	11.09	11.39	11.72	11.87	12.04	12.22	12.40	12.57	12.74	12.90	
10.95	11.19	11.49	11.82	11.97	12.14	12.32	12.50	12.67	12.84	13.00	

# $E_{OP}$ stage pH control: How to do it?

- Safety issue
  - Recommend the use of filtrate extractor
    - Static type with filter screen
    - Piston type with squeeze mat
- Simplify and speed up preventive maintenance
  - Scarcier E&I resources
  - Calibration liquid-liquid

# $E_{OP}$ stage pH control: How to do it?

- Filtrate extractor
  - Allow the use of cheaper pH probe
  - Safe handling of hot filtrate media
  - Faster calibration check
  - Use temperature measurement at pH probe location
    - Beware of built-in temperature measurement, here is it located on the probe
    - Use RTD on filtrate pot
  - Minimize deadtime with location close to pump/mixer
    - Also minimize piping diameter and pipe length to pH pot
  - Look for minimum 200-250ml/min filtrate flow
  - Flush back with combination of steam/hot water/air to avoid scaling deposit of filter screen and temperature shock of pH probe

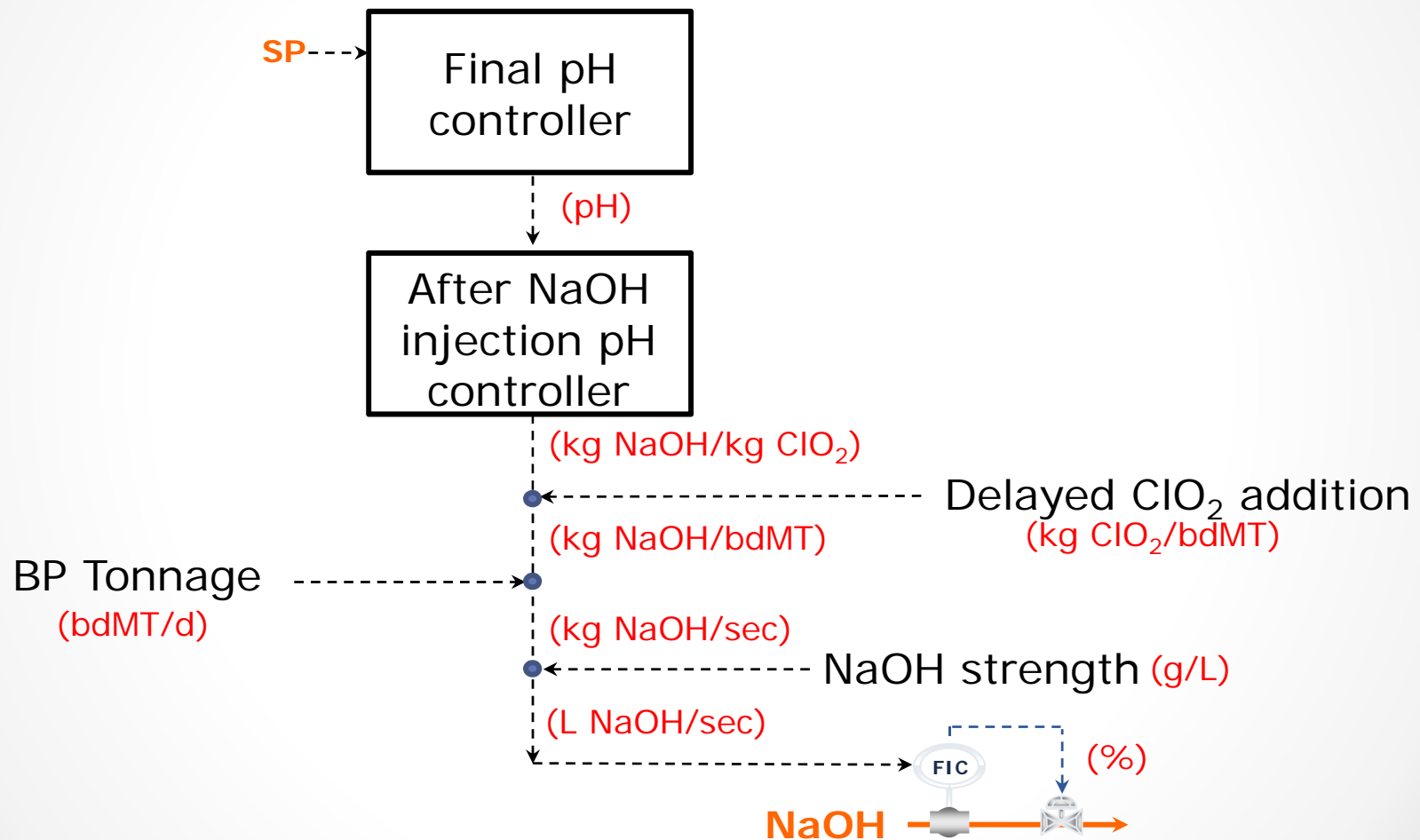
# $E_{OP}$ stage pH control: How to do it?

- pH probe preventive maintenance
  - Weekly
  - Use pH buffer 7 and 10, higher if available
  - Replace probe at fixed date
    - Have a historical tracking of pH probe
    - You may lose your accumulated savings by trying to extend probe life to failure.
  - When replacing a pH probe, always double check the next day. Somehow it needs to “cure in process media”

# $E_{OP}$ stage pH control:

- NaOH dosage is added as kg/ton, lb/ton or % applied
- Monitor/use NaOH/ $ClO_2$  ratio – back up control
  - Indication of potential issues
  - Also used as limiter
- PID controller to be Lambda tune
  - with possible gain schedule on tonnage
- Multiple cascades loop possible
  - End pH is what we're after
    - Achieved by better control of pH early on
  - End pH
    - ph at top of upflow pipe or tube
      - before pressure control valve if present
    - at the bottom of downflow tower some 5 ft above dilution ring
    - in the vat...(because this is where testing is done)

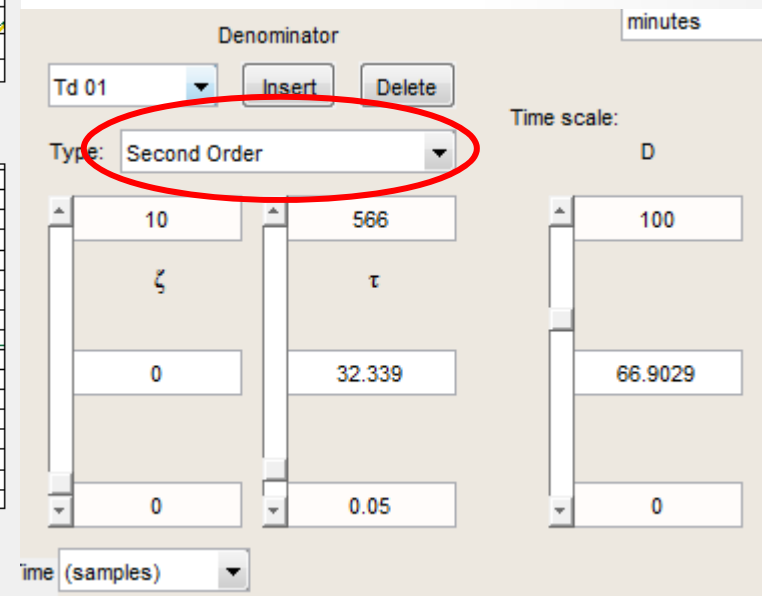
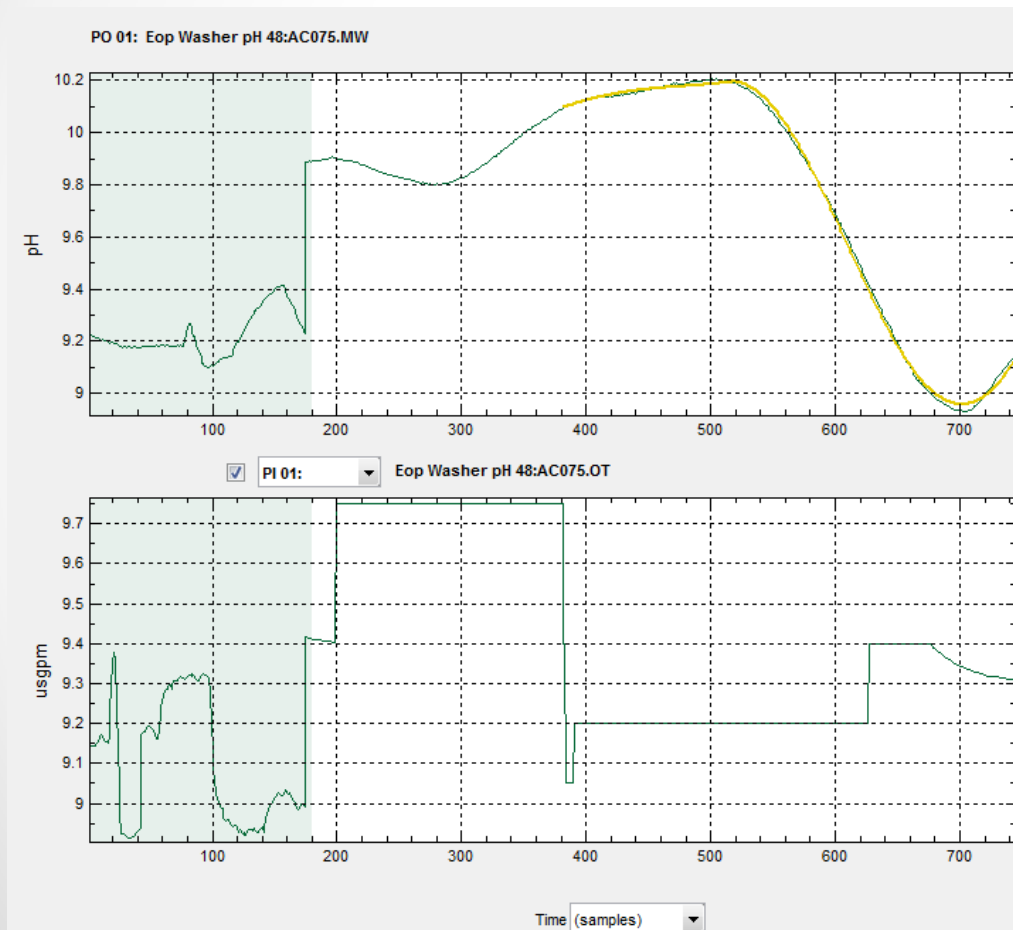
# $E_{OP}$ stage pH control:





# $E_{OP}$ stage pH control: in the vat...

- Deadtime is longer than the residence time(!)
  - Filter tank filters response
- Behave like a second order loop



# $E_{OP}$ stage pH control:

- Multiple cascades loop possible
  - Permissive: time delay for PID on top of upflow tube
  - Permissive: time delay for PID at end of tower
  - Lambda tuned with gain schedule based upon tonnage
- Troubleshooting: when pH loop starts cycling, this is a strong indication pH probe has become insensitive
  - Don't retune the loop!!!
  - Change pH probe.
    - log life times and schedule PM for probe replacement
    - pH probe cost not worth running to failure

# Acknowledgment:

- Doug Reid & AKZO team for all testing on  $E_{Op}$  filtrate, and main author of technical paper: " THE IMPACT OF SAMPLE TEMPERATURE ON pH OF EXTRACTION STAGE FILTRATES "
- Brian LaBrash & team for sharing process data.
- Feedback from the BC participants to make me realize once again that process control engineers need to do a better job at explaining and simplifying control concepts. Too often, process control engineers take basic process control concept for granted.